

Advanced Fluid Mechanics

Transition to Turbulence & Turbulence

Applications to Transfers, Aerodynamics & Wind Energy

General planning:

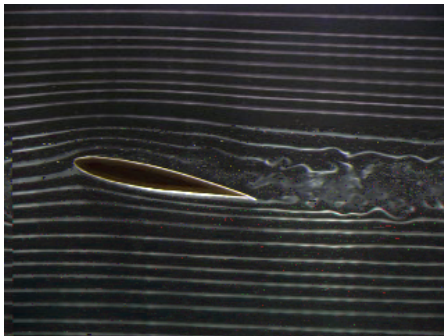
Sess ^o - Man	Date	Content
1 - EP	09/01 m	Thermoconvection with slip boundary conditions
2 - EP	11/01 m	Transfers in thermoconvection with various boundary conditions Patterning, supercritical bifurcations
3 - JP	17/01 m	Wind resources - Conversion principles - Aero
4 - JP	18/01 m	Aero - Wind field and Turbulence
5 - JP	19/01 m	Wind field and Turbulence - Conversion dynamics - Stochastic proc.
JP	19/01 a	General conf.: Turbulence & Wind Energy Research
→ 6 - EP	23/01 m	Aerodynamics: linear stability of an open shear flow
7 - EP	25/01 m	Aerodynamics: nonlinear stability of open shear flows Patterning, subcritical & saddle-node bifurcations
EP	10/02 a	Examination

Today: Session 6: Transition in Open Shear Flows:

- ▶ Introduction: Instabilities of Open Shear Flows, Rayleigh criterion
- ▶ Numerical linear stability analysis of Plane Poiseuille Flow: TS waves

Open Shear Flows are often encountered in Aerodynamics

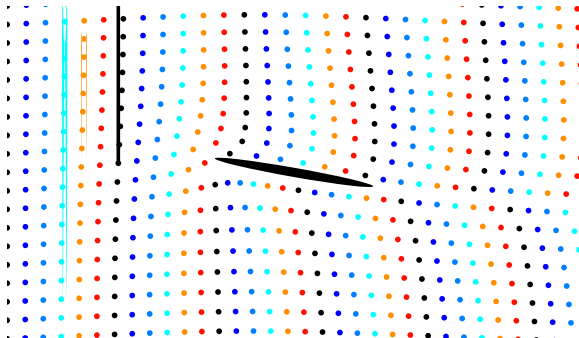
Turbulent Flow around an obstacle, an Airfoil,
observed with smoke in a Wind Tunnel at U. Stanford:



[DVD 'Multimedia Fluid Mechanics', Homsy et al. 2004, Cambridge University Press]

Open Shear Flows are often encountered in Aerodynamics

Laminar Flow around an obstacle, an Airfoil, also exists,
and may be computed with Complex Analysis Techniques:



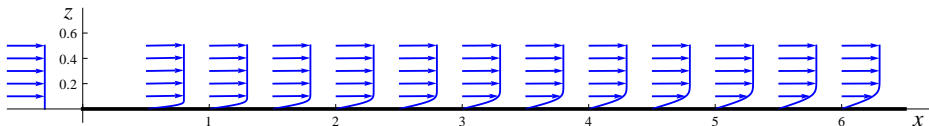
[Plaut E. *Mecanique des fluides*. Cours Mines Nancy 2A]

When and how **Laminar Open Shear Flows** get **unstable** and go to **Turbulence** ?

When and how 2D xz Laminar Open Shear Flows get unstable ?

Example: Blasius Boundary Layer over a flat plate

Aerodynamical case: x and z in meters: $U = 0.1$ m/s :



$$\delta = \sqrt{\frac{\nu x}{U}}, \quad \zeta = \frac{z}{\delta}, \quad v_x = U f'(\zeta), \quad v_z = \frac{1}{2} \sqrt{\frac{\nu U}{x}} [\zeta f''(\zeta) - f(\zeta)]$$

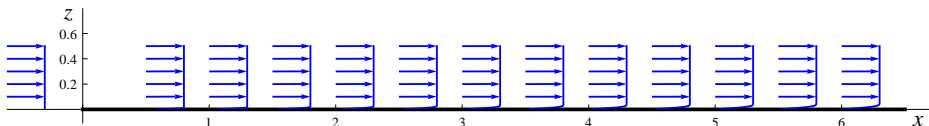
Thickness of the Boundary Layer where $v_x = 0.99U$:

$$\delta_L = 5 \sqrt{\frac{\nu x}{U}} \iff U = 25 \frac{\nu x}{\delta_L^2} \simeq 25 \frac{2 \cdot 10^{-5} \text{ m}^2/\text{s} \cdot 6 \text{ m}}{0.04 \text{ m}^2} \simeq 0.1 \text{ m/s}$$

When and how 2D xz Laminar Open Shear Flows get unstable ?

Example: Blasius Boundary Layer over a flat plate

Aerodynamical case: x and z in meters: $U = 2 \text{ m/s}$:



$$\delta = \sqrt{\frac{\nu x}{U}}, \quad \zeta = \frac{z}{\delta}, \quad v_x = U f'(\zeta), \quad v_z = \frac{1}{2} \sqrt{\frac{\nu U}{x}} [\zeta f''(\zeta) - f(\zeta)]$$

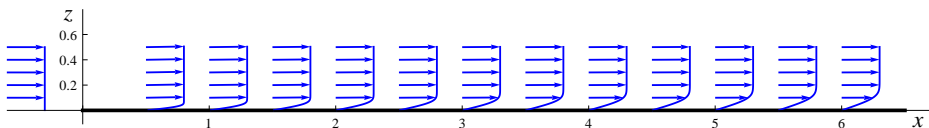
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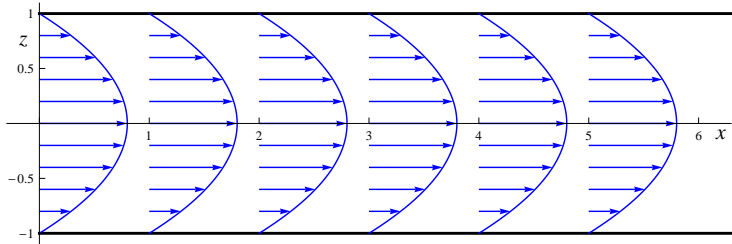
$$\delta = \sqrt{\frac{\nu x}{U}}, \quad \zeta = \frac{z}{\delta}, \quad v_x = U f'(\zeta), \quad v_z = \frac{1}{2} \sqrt{\frac{\nu U}{x}} [\zeta f''(\zeta) - f(\zeta)]$$

Thickness of the Boundary Layer where $v_x = 0.99U$:

$$\delta_L = 5 \sqrt{\frac{\nu x}{U}}$$

When and how 2D xz Laminar Open Shear Flows get unstable ?

Example: Plane Poiseuille Flow



Viscous flow between two plates at $z = \pm h$:

$$\bar{\mathbf{v}} = U(z) \bar{\mathbf{e}}_x = U_0(1 - (z/h)^2) \bar{\mathbf{e}}_x, \quad \bar{\mathbf{p}} = p + \rho g Z = -Gx \quad \text{with} \quad G = 2\eta \frac{U_0}{h^2}.$$

Particular case of **Plane Parallel Flow** !

When and how 2D xz Laminar Open Shear Flows get unstable ?

General Example: Plane Parallel Flows

$$\bar{\mathbf{v}} = \bar{\mathbf{v}}_0 = U(z) \bar{\mathbf{e}}_x, \quad \bar{\mathbf{p}} = p + \rho g Z = 0 \text{ in an inviscid uid,}$$

$$\bar{\mathbf{p}} = p + \rho g Z = -Gx \text{ in a viscous uid,}$$

is solution of the Euler ($\eta = 0$) or Navier-Stokes ($\eta \neq 0$) equation

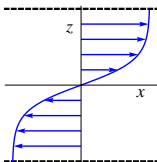
$$\rho \partial_t \bar{\mathbf{v}} + (\bar{\mathbf{v}} \cdot \bar{\nabla}) \bar{\mathbf{v}} = -\bar{\nabla} \bar{\mathbf{p}} + \eta \bar{\Delta} \bar{\mathbf{v}}$$

$$\iff \bar{\mathbf{0}} = G \bar{\mathbf{e}}_x + \eta U''(z) \bar{\mathbf{e}}_x$$

whatever $U(z)$ in an inviscid uid,

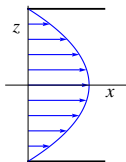
provided $U(z) = \alpha + \beta z + \gamma z^2$ in a viscous uid.

Mixing Layer



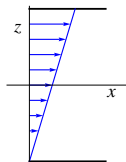
inviscid .

Poiseuille Flow



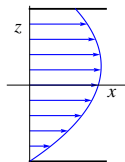
viscous .

Couette Flow



viscous .

Couette-Poiseuille Flow



viscous .

Stability Analysis of Plane Parallel Flows

Basic flow:

$$\bar{\mathbf{v}}_0 = U(z) \bar{\mathbf{e}}_x, \quad \bar{p}_0 = p_0 + \rho g Z = -Gx \quad \text{with} \quad \begin{array}{l} G = 0 \text{ in an inviscid fluid,} \\ G > 0 \text{ in a viscous fluid.} \end{array}$$

Basic flow with **perturbations**:

$$\bar{\mathbf{v}} = \bar{\mathbf{v}}_0 + \bar{\mathbf{u}}, \quad \bar{p} = \bar{p}_0 + p^0$$

$$\partial_t \bar{\mathbf{v}} + (\bar{\mathbf{v}} \cdot \bar{\nabla}) \bar{\mathbf{v}} = -(1/\rho) \bar{\nabla} \bar{p} + \nu \bar{\Delta} \bar{\mathbf{v}} \quad (\text{NS})$$

$$\partial_t \bar{\mathbf{u}} + U^0 u_z \bar{\mathbf{e}}_x + U \partial_x \bar{\mathbf{u}} + (\bar{\mathbf{u}} \cdot \bar{\nabla}) \bar{\mathbf{u}} = -(1/\rho) \bar{\nabla} p^0 + \nu \bar{\Delta} \bar{\mathbf{u}} \quad (\text{NS})$$

$$\text{div} \bar{\mathbf{v}} = 0 \quad (\text{MC})$$

$$\text{div} \bar{\mathbf{u}} = 0 \quad (\text{MC})$$

▷ Unit of length = h half-width of the channel, thickness of the mixing layer...

▷ Unit of velocity = $U_0 = \max_z U(z)$ scale of U

▷ Unit of time = h/U_0 advection time

$$\partial_t \bar{\mathbf{u}} + U^0 u_z \bar{\mathbf{e}}_x + U \partial_x \bar{\mathbf{u}} + (\bar{\mathbf{u}} \cdot \bar{\nabla}) \bar{\mathbf{u}} = -\bar{\nabla} p^{00} + R^{-1} \bar{\Delta} \bar{\mathbf{u}} \quad (\text{NS})$$

with the **Reynolds number** $R = U_0 h / \nu$, $R = \infty$ in an inviscid fluid.

2D xz Stability Analysis of Plane Parallel Flows

Dimensionless equations for the **perturbations** $\bar{\mathbf{u}}$ of velocity and p^{00} of pressure:

$$\partial_t \bar{\mathbf{u}} + U^0 u_z \bar{\mathbf{e}}_x + U \partial_x \bar{\mathbf{u}} + (\bar{\mathbf{u}} \cdot \bar{\nabla}) \bar{\mathbf{u}} = -\bar{\nabla} p^{00} + R^{-1} \bar{\Delta} \bar{\mathbf{u}}, \quad (\text{NS})$$

$$\text{div} \bar{\mathbf{u}} = 0. \quad (\text{MC})$$

2D xz perturbations can be defined by their **streamfunction** $\psi(x, z)$:

$$\bar{\mathbf{u}} = \overline{\text{curl}}(\psi \bar{\mathbf{e}}_y) = (\bar{\nabla} \psi) \times \bar{\mathbf{e}}_y = -(\partial_z \psi) \bar{\mathbf{e}}_x + (\partial_x \psi) \bar{\mathbf{e}}_z.$$

How can one eliminate p^{00} in (NS) ? Consider $\overline{\text{curl}}(\text{NS}) \cdot \bar{\mathbf{e}}_y$ i.e. the **vorticity equation**:

$$\partial_t (-\psi) + \partial_z \bar{\mathbf{u}} \cdot \bar{\nabla} u_x - \partial_x \bar{\mathbf{u}} \cdot \bar{\nabla} u_z = R^{-1} (-\psi) + U \partial_x (-\psi) - U^{00} (\partial_x \psi). \quad (\text{Vort})$$

$$\boxed{D \cdot \partial_t \psi = L_R \cdot \psi + N_2(\psi, \psi)}. \quad (\text{Vort})$$

Boundary conditions:

$$\text{Viscous fluid : } \bar{\mathbf{u}} = \bar{\mathbf{0}} \iff \partial_x \psi = \partial_z \psi = 0 \quad \text{if } z = z_0,$$

$$\text{Inviscid fluid : } u_z = 0 \iff \partial_x \psi = 0 \quad \text{if } z = z_0.$$

2D xz Linear Stability Analysis of Plane Parallel Flows

$$\boxed{D \cdot \partial_t \psi = L_R \cdot \psi} \quad (\text{Vort})$$

$$D \cdot \partial_t \psi = - \partial_t \psi, \quad L_R \cdot \psi = R^{-1} (-\psi) + U \partial_x (\psi) - U^{(0)} (\partial_x \psi),$$

$$\text{Viscous uid: } \bar{\mathbf{u}} = \bar{\mathbf{0}} \iff \partial_x \psi = \partial_z \psi = 0 \quad \text{if } z = z_c,$$

$$\text{Inviscid uid: } u_z = 0 \iff \partial_x \psi = 0 \quad \text{if } z = z_c.$$

Normal mode analysis:

$$\psi = n(z) \exp(ikx + \sigma t) = n(z) \exp[ik(x - c_r t)] \exp(kc_i t)$$

with $k =$ **horizontal wavenumber**, $k \neq 0$, n another label to mark normal modes,
 $\sigma =$ **temporal eigenvalue**.

Most often the bulk velocity of the basic flow $\langle U \rangle_z > 0 \Rightarrow$ by advection

$$\sigma = -i\omega = -ikc \quad \text{with } c \text{ the } \mathbf{complex \ phase \ velocity},$$

$$c_r > 0 \text{ the } \mathbf{real \ phase \ velocity},$$

$kc_i > 0$ (resp. < 0) the **growth rate** (resp. damping rate).

2D xz Linear Stability Analysis of Plane Parallel Flows

$$-\sigma \psi = R^{-1} (-\psi) + U \partial_x (\psi) - U'' (\partial_x \psi) \quad (\text{Vort})$$

$$\iff ikc \psi = R^{-1} (-\psi) + ikU \psi - ikU'' \psi \quad (\text{Vort})$$

$$\iff \boxed{(U - c) \psi - U'' \psi = (ikR)^{-1} \psi} \quad (\text{Vort})$$

Orr - Sommerfeld eq. in a viscous uid, **Rayleigh eq.** in an inviscid uid ($R = \infty$)

B.C. at $z = z_0$: Viscous uid: $\psi = \partial_z \psi = 0$; Inviscid uid: $\psi = 0$.

Normal mode analysis:

$$\psi = \psi_n(z) \exp(ikx + \sigma t) = \psi_n(z) \exp[ik(x - c_r t)] \exp(kc_i t)$$

with $k =$ **horizontal wavenumber**, $k \neq 0$, n another label to mark normal modes,
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2D xz Linear Stability Analysis of Inviscid Plane Parallel Flows

Normal mode analysis: assume there is at least one **amplified mode**

$$\psi = \psi(z) \exp(ikx - ikct) = \psi(z) \exp[ik(x - c_r t)] \exp(kc_i t)$$

with c_r the **real phase velocity**, $kc_i > 0$ the **growth rate**.

It satisfies the **Rayleigh equation**

$$(U - c) \psi'' - U'' \psi = 0$$

with the B.C. $\psi = 0$ if $z = z_{\pm}$.

Exercise 2.1 Rayleigh's inflection point criterion

▷ Express $\psi''(z)$ as a function of $\psi(z)$, $U(z)$, $U''(z)$, k and c .

▷ By multiplication with a suitable function and integration over $z \in [z_-, z_+]$, show that

$$\int_{z_-}^{z_+} k^2 |\psi(z)|^2 + |\psi''(z)|^2 dz + \int_{z_-}^{z_+} \frac{U''(z) |\psi(z)|^2}{U(z) - c} dz = 0$$

and

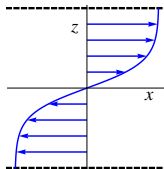
$$\int_{z_-}^{z_+} \frac{U''(z) |\psi(z)|^2}{|U(z) - c|^2} dz = 0 \Rightarrow \text{if } U'' \neq 0, U'' \text{ must change sign somewhere,}$$

there must exist an **inflection point** in the U -profile.

Instability of an Inviscid Plane Parallel Flow, the Mixing Layer

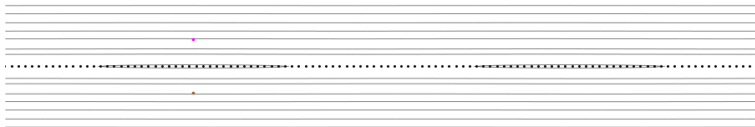
The Hyperbolic Tangent **Mixing Layer**

$$\bar{\mathbf{v}}_0 = U_0 \tanh(z/h) \bar{\mathbf{e}}_x$$



displays a **Kelvin-Helmholtz Instability** !

Initial condition $\bar{\mathbf{v}} = \bar{\mathbf{v}}_0 + \bar{\mathbf{u}}$ with $\bar{\mathbf{u}}$ small:

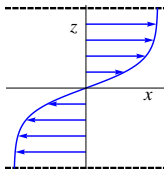


[Plaut E. *Mécanique des fluides*. Cours Mines Nancy 2A]

Instability of an Inviscid Plane Parallel Flow, the Mixing Layer

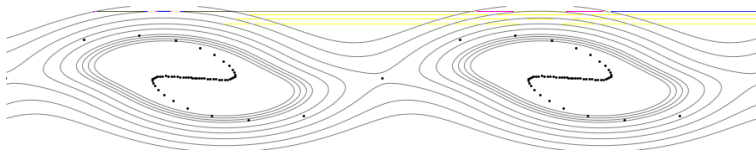
The Hyperbolic Tangent **Mixing Layer**

$$\bar{\mathbf{v}}_0 = U_0 \tanh(z/h) \bar{\mathbf{e}}_x$$



displays a **Kelvin-Helmholtz Instability** !

Time development: the perturbation $\bar{\mathbf{u}}$ becomes large !

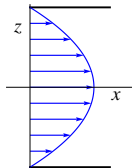


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Stability of Inviscid Plane Poiseuille Flow

Plane Poiseuille Flow of an Inviscid Fluid has no inflection point \Rightarrow it is **stable**.

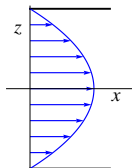
$$\bar{\mathbf{v}}_0 = U_0(1 - (z/h)^2) \bar{\mathbf{e}}_x$$



Stability of Viscous Plane Poiseuille Flow

Plane Poiseuille Flow of a Viscous Fluid might be **unstable** ?

$$\bar{v}_0 = U_0(1 - (z/h)^2) \bar{e}_x$$



Must calculate normal modes

$$\psi = \psi(z) \exp(ikx + \sigma t) = \psi(z) \exp[ik(x - c_r t)] \exp(kc_i t)$$

by solving the **Orr - Sommerfeld equation**

$$\sigma D\psi = -\sigma \psi = L_R \psi = -R^{-1} \psi + ik(U \psi - U''\psi)$$

with the B.C. at $z = \pm 1$: $\psi = \partial_z \psi = 0$.

Eigenvalue $\sigma = -ikc_i$; $c_r = -\sigma_i/k$ phase velocity ;

$\sigma_r > 0$	\leftrightarrow	amplified mode
$\sigma_r = 0$	\leftrightarrow	neutral mode
$\sigma_r < 0$	\leftrightarrow	damped mode

Exercise 2.2

Stability of Viscous Plane Poiseuille Flow: Ex. 2.2

$$\sigma D = -\sigma = L_R = -R^{-1} + ik(U - U^{(0)}) \quad (\text{OS})$$

with

$$= -k^2 + \frac{d^2}{dz^2}$$

and the boundary conditions

$$= \theta = 0 \quad \text{if} \quad z = \pm 1 .$$

Spectral expansion

$$\chi(z) = \sum_{n=1}^N F_n(z)$$

with

$$F_n(z) = (z-1)^2 (z+1)^2 T_{2n-2}(z) = (z^2-1)^2 T_{2n-2}(z)$$

Evaluate (OS) at the **Gauss-Lobatto collocation points**

$$\Leftrightarrow \sigma \sum_{n=1}^N DF_n(z_m) = \sum_{n=1}^N LF_n(z_m) \Leftrightarrow \sigma MD \cdot V = ML \cdot V$$

$$\text{with} \quad V = (1, \dots, N)^T, \quad MD_{mn} = DF_n(z_m), \quad ML_{mn} = LF_n(z_m).$$